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#### (54) PROCESS FOR THE MANUFACTURE OF CONCENTRATED LIQUID DYEING PREPARATIONS OF LOW SALT CONTENT

We, CIBA-GEIGY A.G., a Swiss body corporate of Basle, Switzerland, do hereby declare the invention for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:-

The present invention relates to a process for the manufacture of concentrated, liquid dyeing preparations of low salt content, especially preparations of water-

soluble dyestuffs and optical brighteners.

Disperse dyestuffs, and above all water-soluble anionic and cationic dyestuffs and optical brighteners are usually separated out by salting-out of the reaction solution, for example with sodium chloride, potassium chloride or ammonium sulphate. In doing so, it is often very difficult to cause the dyestuff or optical brightener to separate out in a form which is easy to filter. In most cases, but not always, it is advantageous to effect the precipitation at approx. 70 to 80° C., and more rarely at the boil. By doing this, it is frequently possible to convert initially gelatinous precipitates into a crystalline or granular form. Apart from the precipitation temperature and the salt concentration, the pH value of the solution is sometimes also of importance as regards the character of the precipitate. For example, it sometimes happens that a precipitate which is easy to filter is only obtained over quite specific pH ranges.

Dyestuff salts or optical brightener salts which are still very soluble even in saturated salt solution must be isolated by, for example, evaporating the solution

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The dyestuffs or optical brighteners obtained by salting out and subsequent filtration, or by evaporating the coupling solution, condensation solution and/or neutralisation solution, in most cases have a high salt content. Dyeing preparations having a high salt content are frequently undesirable since, for example, they have too low a solubility, especially too low a solubility in cold water. Desalinating products containing salt, in practice, presents great difficulties, is expensive and in many cases leads to gelatinous pseudo-solutions which cannot be filtered.

Salting out, e.g. by dissolving and reprecipitating using organic solvents, is possible but complicated. Dialysis (artificial kidney) methods are also possible, but

are very cumbersome and require large quantities of liquid. Moreover, dyestuffs which have been isolated by salting out often contain low molecular coloured or colourless compounds, e.g. diazo and coupling components, monocondensates and hydrolysed sulphonic acid chlorides as impurities which are usually very difficult to isolate or at least must be isolated by chromatographic methods.

A process has now been found according to the present invention, which makes is possible to concentrate liquid dyeing preparations and reduce their salt content, especially to give impurity-free preparations of water-soluble dyestuffs and optical brighteners, in a simple manner so as to avoid all the abovementioned difficulties and disadvantages. According to the present invention, there is provided a process for concentrating, and reducing the salt content of, a liquid dyeing or optical brightening preparation which comprises passing a salt-containing solution or suspension of at least one dyestuff or optical brightening agent at least once, under pressure, over

[Price 25p]

a semipermeable membrane, which allows water and salt dissolved therein to pass through while retaining the dyestuff or optical brightening agent. In contrast to the customary filtration, wherein solid particles are separated from liquids, the membrane-ultrafiltration process represents a selective molecular separation method. 5 The semi-permeable membranes act as molecular sieves, which retain dissolved substance at the membrane interface, with the molecular weight being the factor which decides retention or separation ("cut off levels"). Advantageously, membranes are employed which have a "cut off level" having at least 90% retention when they 10 are subjected to a continuous ultrafiltration for 20 to 30 minutes. This membrane-10 ultrafiltration process is, of course, related to reverse osmosis wherein the molecular size of the substance or substances dissolved in the solution and of water must be in a certain size ratio to one another. Semi-permeable membranes which can be used according to the present invention should ensure a high transmission of water and salts, such as sodium chloride, 15 15 potassium chloride, ammonium sulphate, sodium phosphate, potassium sulphate, sodium acetate, and impurities, such as uncondensed or partially decomposed starting materials, which have a relatively low molecular weight. Additionally, however, they should also be sufficiently stable to suffer as little wear as possible in operation. These 20 requirements are for example met by anisotropic, polymeric membranes, which 20 consist of a very thin (for example 0.1 to 1.5 micron thick) layer having an extremely fine-pored texture (for example 2 to 100  $\lambda$  diameter holes) on a much thicker layer (for example 50 to 250 microns thick) of an open-cell, porous plastic (sponge). The thin layer (skin) together with the porous substrate provide a combination of selectivity and high transmission, wherein blockages only occur rarely. 25 25 Semi-permeable membranes of cellulose acetate are preferred, but with these pH values of 3 to 9 should be maintained so as to avoid a degradation (hydrolysis) of the membrane as far as possible. Anisotropic (skin-layer) membranes of biologically inert, "non-cellulosic", synthetic polymers, such as nylon, but also poly-(vinyl isobutyl 30 ether), poly-(ethyl acrylate), poly-tetrahydrofurane, poly-(triallyl phosphate), poly-30 (vinyl methyl ketone) and cellulose di- or tri-acetate, are very resistant because of their thermal, chemical and physical properties. They generally withstand temperatures of up to 200° C. and can be exposed to acids, alkali or oxidising agents without suffering damage. These membranes show a "cut off level" of molecular weight 300 35 to 10,000. For the process according to the present invention, membranes with a 35 "cut off level" of molecular weight 400 to 1000 are particularly suitable. They permit the permeation of water, optionally mixed with organic solvents and dissolved substances, which because of their molecular sizes lie below the cut off level, at high speeds per unit area and at relatively low pressures. According to the invention, pressures of 3 to 100, and preferably 20 to 50 atmospheres generally suffice. The pressure can, for 40 40 example, be exerted by means of compressed air or of a pump. Naturally the cut off level must be such as to retain substantially all of the dyestuff or optical brightener; it will, of course, be appreciated that the process of this invention will only work satisfactorily if the molecular weight of the dyestuff is higher than that of the salts but this is nearly always the case. 45 45 In an ultrafiltration pass, the salting-out effect can be up to 70 per cent or more, without losses of dyestuff. During this, the volume of the solution of the retained substances above the membrane correspondingly decreases and the concentration of the retained particles increases. If a further reduction in the salts and other substances 50 of low molecular weight is desired, this can be achieved without difficulties, after dilut-50 ing the retained solution or suspension with water, preferably to the initial volume, by repeating the process once or several times. The ultrafiltration can also be carried out continuously, by matching the speed of supply of the water to the speed of removal of the ultrafiltrate. Salting-out and purifying effects of up to 95%, or, if desired, even up to 99%, that is to say until the ultrafiltrate is free of undesired substances, can 55 be achieved discontinuously and continuously in this simple manner. Possible dyestuffs to which the process of this invention is applicable include disperse dyestuffs and, above all, water-soluble anionic and cationic dyestuffs, in particular monoazo, disazo or polyazo dyestuffs, formazane, anthraquinone, nitro, 60 methine, styryl, azastyryl, naphthoperinone, quinophthalone or phthalocyanine dye-60

> The water-soluble anionic dyestuffs which preferably are used according to the present invention, are especially the alkali salts or ammonium salts of the so-called acid wool dyestuffs, of the reactive dyestuffs or of the substantive cotton dyestuffs of

The resulting concentrated, liquid dyeing preparations of low salt content can, if desired, be concentrated further, for example in vacuo, or can even be evaporated to dryness. Easily soluble products which are free of the hitherto customary fillers, can thereby be obtained in an extremely simple manner.

such as urea, dextrin, glucose and diethylene glycol to the concentrates which have

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Thus it is possible by the process according to the invention in a simple manner to produce substances which are pure enough for photographic and drawing materials such are used for pressure copying. Dyestuffs for photographic purposes, e.g. dyestuffs of the azo series used for photographic prints, must be practically completely free

The Examples which follow further illustrate the present invention

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Example 1.

360 g of moist dyestuff press cake, containing 120 g of dyestuff of the formula

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$$\sum_{SO_3H} N - N - N - N + CONH - CH_3 - N - N - SO_3H$$

are suspended in 1500 ml of water, and the dyestuff suspension containing about 15% of sodium chloride is continuously ultra-filtrated at room temperature, whilst constantly supplying an amount of water corresponding to the ultrafiltrate, and using a semi-permeable cellulose acetate membrane having a "cut off level" of molecular weight 400, and a pressure of 35 kg/cm² (500 lb per square inch). After removing 95% of the theoretical amount of sodium chloride (measured from salt content of the ultrafiltrate) from the original suspension, without loss of dyestuff, which is achieved by passage of 4000 ml of water, the supply of water is stopped, and after concentrating the dyestuff solution to a volume of 600 ml the ultrafiltration is stopped.

The dyestuff solution thus obtained can be concentrated in vacuo to a volume of 300 ml, whereby an intensely coloured and directly usable dyeing preparation is obtained, which is stable, with the dissolved dyestuff showing no tendency to separate out. To obtain a commercial preparation which is storage stable for a long period, advantageously 5% by weight of urea or diethylene glycol are added to the concentrate.

Pouring the preparation into warm water and adding the auxiliaries customary in dyeing yields a directly usable liquor for dyeing cellulose fibres, especially paper, in yellow colour shades.

If in the above Example, the dyestuff of the press cake is replaced by corresponding amounts of the substantive dyestuffs indicated in Table I below, column 2, and in other respects the procedure indicated in the Example is followed, directly ready-to-use and storage-stable dyeing preparations are again obtained, which dye cellulose fibres in the colour shades indicated in the last column.

TABLE I

Example No.	Dyestuff	Colour shade on cellulose fibres
2	H <sub>2</sub> N 0 - Cu - 0 0 - Cu - 0 NH <sub>2</sub> N - N - N - N - N - N - N - N - N - N -	blue
3	OH OH N=N-N-NHCOCH3	scarlet
4	NaO <sub>3</sub> S H <sub>2</sub> M OH CH <sub>3</sub> O OCH <sub>3</sub> HO NH <sub>2</sub> SO <sub>3</sub> Na SO <sub>3</sub> Na	blue
5	H <sub>2</sub> N — N — N — N — N — NH <sub>2</sub> CH <sub>3</sub> CH <sub>3</sub>	brown
6	N-C-N-N-N-N-C-N-N-N-C-N-C-N-C-N-C-N-C-N	yellow
7	SO <sub>3</sub> Na CH <sub>3</sub> SO <sub>3</sub> Na SO <sub>3</sub> Na SO <sub>3</sub> Na	yellow
8	NaO <sub>3</sub> S — N — N — N	orange
9	NH2 N - N - N - N H2	brown

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Concentration of the dyeing preparations, obtainable according to Examples 1 to 9, in vacuo to a volume of 300 ml or to dryness, yields extremely easily water-soluble dyestuff preparations of low salt content.

Example 10. 150 g of the dyestuff of the formula

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which has been isolated by salting-out, and dried, are dissolved in 3000 ml of water at 70° C., and the solution containing about 10% of sodium chloride is cooled to room temperature and ultrafiltered by means of a semi-permeable polyamide membrane with a "cut off level" of molecular weight 450, and a pressure of 10 kg/cm², and is simultaneously concentrated to a volume of 250 ml. A concentrated, stable, directly ready-to-use dyestuff solution is thus obtained. After pouring the preparation into water and adding the auxiliaries customary in dyeing, a directly usable liquor for dyeing wool in red colour shades is obtained.

If in the above Example, the dyestuff is replaced by corresponding amounts of the dyestuffs indicated in Table II below, column 2, and in other respects the procedure indicated in the Example is followed, directly ready-to-use and storage-stable dyeing preparations are again obtained, which dye wool and synthetic polyamide in the colour shades indicated in the last column of the table.

TABLE II

Example No.	Dyestuff	Colour shade on wool and synthetic polyamide
11	н <sub>3</sub> с — So <sub>2</sub> o — N — N — с — с — с — с н <sub>3</sub> но — с п So <sub>3</sub> н	yellow
12	2:1 cobalt complex  C <sub>2</sub> H <sub>5</sub> SO <sub>2</sub> N-N-C-C-C-CH <sub>3</sub> OH HO-C-N  Ct	yellow
13	SO <sub>2</sub> NH <sub>2</sub> SO <sub>2</sub> N N N N N N N N N N N N N N N N N N N	green

## TABLE II (Continued)

Example No.	Dyestuff	Colour shade on wool and synthetic polyamide
14	4.4'-bis-(o-diazophenyl-sulphonyloxy)-diphenylmethane	yellow
, 15	4.4'-bis-(o-diazophenyl-sulphonyloxy)-diphenylmethane2-aminonaphthalene-5-sulphonic acid (2 equivalents)	orange
16	4.4'-bis-(o-diazophenyl-sulphonyloxy)-diphenylmethane	red
17	0 NH <sub>2</sub> SO <sub>3</sub> H 0 NH —	blue
18	O NH <sub>2</sub> SO <sub>3</sub> H HO <sub>3</sub> S + H <sub>2</sub> M O O NH - O HN O	blue
19	но но <sub>3</sub> s- so <sub>3</sub> н	scarlet
20	SO <sub>2</sub> NH <sub>2</sub> N <sub>2</sub> N <sub>3</sub> N <sub>3</sub> N <sub>3</sub> N <sub>3</sub> N <sub>3</sub>	blue

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### TABLE II (Continued)

Example No.	Dyestuff	Colour shade on wool and synthetic polyamide
21	HO <sub>3</sub> S N - N - N	black - after chroming

Example 22. 900 g of a moist press cake, which contains 500 g of the dyestuff of the formula

are introduced into 5000 ml of water, whilst stirring, and the resulting dyestuff 5 solution is continuously ultrafiltered at room temperature with constant supply of 5 an amount of water corresponding to the ultrafiltrate, and using a semi-permeable cellulose acetate membrane with a "cut off level" of molecular weight 500 and a pressure of 25 kg/cm<sup>2</sup>; after a passage of 10000 ml of water no chloride ions or not-10 acylated starting material are detectable in the ultrafiltrate. Thereafter, the supply of 10 water is switched off and the dyestuff solution is concentrated to a volume of 1000 ml. The dyeing preparation thus obtained is very stable and directly ready to use. On stirring the preparation into water, and after adding thickeners and the auxiliaries which are customary in dyeing, a printing paste for printing natural or regenerated 15 cellulose fibres is obtained. 15 If instead of the abovementioned press cake, the coupling solution of the dyestuff of the above formula, obtained by coupling diazotised 1-aminobenzene-2-sulphonic acid with 1-(2,4,5-trichloropyrimidylamino)-8-hydroxynaphthalene-3,6-disulphonic acid, is used, and in other respects the procedure indicated in the Example is followed, a 20 dyeing preparation with similarly good properties is obtained. 20 If, in the above Example, the dyestuff in the press cake is replaced by corresponding amounts of the reactive dyestuffs indicated in Table III, below, column 2, and in other respects the procedure indicated in the Example is followed, directly ready-to-use and storage-stable dyeing preparations are again obtained, which dye natural or regenerated cellulose in the colour shades indicated in the last column of the table. 25

### TABLE III

<del></del>		
Example No.	Dyestuff	Colour shade on natural and regenerated cellulose
23	- CI OH HO3S - NH-CCHC-CI	greenish-tinged yellow
24	O NH2 SA3H O NH————————————————————————————————————	blue
25	OH N-CO-CH-C-CH <sub>3</sub> SO <sub>3</sub> H SO <sub>3</sub> H	orange
26	(HO3S)3-{CuPc}-SO2-NH-CNH-CNH-CNH-CCI	turquo: se
	(wherein CuPc denotes the copper phthalocyanine radical)	

#### TABLE III (Continued)

Example No.	Dyestuff	Colour shade on natural and regenerated cellulose
27	наз — кно —	claret
28	SQ3N HO N-N-N-CO- SQ2CN3	orange
29	$\begin{bmatrix} Cu Pc & + SO_3 N)_2 \\ + SO_2 NH_2 & + C N - C N \\ + O_3 S & + C CI \end{bmatrix}$	turquoise
30	SO3 Ma OH NH-C N-C N-C NAO3 S SO3 Ma	red

Example 31. 360 g of moist press cake, which contains 120 g of the dyestuff of the formula

$$\begin{bmatrix} \mathsf{CH_{3}O} & & & \\ & \mathsf{C}_{\mathsf{C}}\mathsf{H_{5}} \\ & & \mathsf{C}_{\mathsf{C}}\mathsf{H_{5}} \end{bmatrix}^{\bigoplus} \mathsf{ZnCl_{3}^{\scriptsize \textcircled{\tiny O}}}$$

5 are introduced into 2000 ml of water, whilst stirring, and the resulting dyestuff solution is continuously ultrafiltered, with constant supply of an amount of water corresponding to the ultrafiltrate, and using a semi-permeable cellulose triacetate membrane having a

"cut off level" of molecular weight 1000, and a pressure of 10 kg/cm<sup>2</sup>, until chloride ions are no longer detectable in the ultrafiltrate. Thereafter, the supply of water is switched off and the dyestuff solution is concentrated to a volume of 250 ml.

The dark blue, concentrated dyestuff solution manufactured in this manner is

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storage-stable and directly ready to use. On pouring the preparation into a 100-fold amount of cold or warm water and adding auxiliaries which are customary in dyeing, a directly usable liquor for dyeing acrylonitrile fibres from a short bath is obtained.

If, in the above Example, the dyestuff in the press cake is replaced by corresponding amounts of the cationic dyestuff salts indicated in Table IV below, column 2, and in other respects the procedure indicated in the Example is followed, directly ready-to-use and storage-stable dyeing preparations are again obtained, which dye polyacrylonitrile fibres in the colour shades indicated in the last column of the table.

TABLE IV

Example No.	Cationic dyestuff salts	Colour shade on polyacrylo- nitrile fibres
32	N(CH3) <sup>5</sup> H <sup>2</sup> C−HN−○ Cl⊖ N(CH3) <sup>5</sup>	violet ' ;
33	(H <sub>3</sub> C) <sub>Z</sub> M CS CI <sup>©</sup>	blue
34	CH <sub>3</sub> OCH <sub>3</sub> HO CH <sub>3</sub> HO CH <sub>3</sub> CH <sub>3</sub> CI CH <sub>3</sub> CH <sub>3</sub> CI	scarlet
35	02N - CI	orange
36	H <sub>3</sub> CO	blue

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# TABLE IV (Continued)

Example No.	Cationic dyestuff salts	Colour shade on polyacrylo- nitrile fibres
37	C2HSN-COCO CH3	brilliant yellow
38	CN - CH2 - CO - N - N - S CI Θ	yellow
39	H <sub>3</sub> C CH <sub>3</sub> OCH <sub>3</sub> OCH <sub>3</sub> SO <sub>4/2</sub> OCH <sub>3</sub> SO <sub>4/2</sub>	yellow
40	CI CH3 CH3	pink
41	CH <sub>3</sub> CH — N⊕ HN	red

Example 42.
1.5 kg of moist filter cake, containing 450 g of optical brightener of the formula

are introduced into 5000 ml of water, whilst stirring, and the resulting brightener suspension is ultrafiltered at room temperature, using a semi-permeable membrane of cellulose diacetate having a "cut off level" of molecular weight 500, and a pressure of 20 kg/cm<sup>2</sup>. After removing 5000 ml of ultrafiltrate, the brightener suspension is diluted with 5000 ml of water and again ultrafiltered.

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The concentrated optical brightener preparation obtained in this manner is storage-stable and directly ready to use. On pouring a calculated amount of the preparation into water and adding auxiliaries which are customary in dyeing, a directly usable liquor for brightening natural and regenerated cellulose is obtained.

If, in the above Example, the optical brightener is replaced by corresponding amounts of the optical brighteners indicated in Table V below, column 2, and in other respects the procedure indicated in the Example is followed, directly ready-to-use and storage stable brighteners processed are again obtained.

and storage-stable brightener preparations are again obtained.

TABLE V

TABLE V				
Example No.	Optical brightener			
43 '	HC-CH M			
44	CH-CH-CH-NNN			
45	MSC2HN NC-NC-NH-CH-CH-CH-CH-CNN-CCNHC2HS SO3Na SO3Na			
46	CH-CH-CH-CH-CH-CH-SO <sub>3</sub> Na			
47	CH -			
48	SO3NA			

## TABLE V (Continued)

Example No.	Optical brightener
49	HOCH <sub>2</sub> CH <sub>2</sub> CH <sub>2</sub> CH <sub>3</sub>
50	SO <sub>3</sub> Na
51	SO <sub>3</sub> Na NH-C NH-C NH-C NH-C NH-C NH-C NH-C NH-C

Example 52. 100 g of moist filter cake, containing 36 g of the dyestuff of the formula

are introduced in 3500 ml of water whilst stirring and the resulting dyestuff suspension containing 8 g of the dyestuff base of the formula

is continuously ultrafiltered with constant supply of an amount of water corresponding to the ultrafiltrate at room temperature, using a semi-permeable membrane of cellulose acetate having a "cut off level" of molecular weight 10,000 and a pressure of 7

5	kg/cm After a passage of 18,000 ml of water no dyestuff base of the above formula is detectable in the ultrafiltrate, identified by using a thin layer chromatographic analyse Every 15 minutes 400 ml of ultrafiltrate passed through the semi-permeable membrane. Thereafter, the supply of water is switched off and the dyestuff solution is concentrated to a volume of 500 ml, which concentrate has been evaporated in vacuo to dryness, yielding an extremely pure, highly concentrated, easily water-soluble dyestuff preparation, which can directly be used for photographic prints.	5
10	WHAT WE CLAIM IS:—  1. Process for concentrating, and reducing the salt content of, a liquid dyeing or optical brightening preparation which comprises passing a salt-containing solution or suspension of at least one dyestuff or optical brightening agent at least once, under pressure, over a semi-permeable membrane, which allows water and salt dissolved therein to pass through while retaining the dyestuff or optical brightening agent.	10
15	2. Process according to claim 1 in which the dyestuff is a water-soluble anionic dyestuff.  3. Process according to claim 1 or 2 in which the preparation is a solution resulting from a coupling condensation or proventions.	15
20	ing from a coupling, condensation or neutralisation reaction.  4. Process according to any one of claims 1 to 3 in which the preparation is a slurry of a moist press or filter cake of at least one dyestuff or optical brightener in water.	20
	5. Process according to any one of the preceding claims in which the semi-permeable membrane is of cellulose acetate.  6. Process according to any one of claims 1 to 5 in which the semi-permeable	
25	membrane has a molecular weight "cut off" of 300 to 10,000.  7. Process according to claim 6 in which the semi-permeable membrane has a molecular weight "cut off" of 400 to 1000.  8. Process according to any one of the preceding claims in which the preparation	25
30	is an aqueous solution or suspension which contains 2 to 50% by weight of dyestuff or optical brightener.  9. Process according to any one of the preceding claims in which a pressure of 3	20
	10. Process according to claim 1 substantially as hereinbefore described.  11. Process according to claim 1 substantially as described in any one of Examples.	30
35	1 to 7, 11 to 28, 31 to 36, 38, 39, 42 and 43.  12. Process according to claim 1 substantially as described in any one of Examples 8, 9, 10, 29, 30, 37, 40, 41 and 44 to 52.  13. A liquid dyeing or optical brightening preparation whenever obtained by a	35
40	process as claimed in any one of claims 1 to 12.  14. A preparation according to claim 13 which is concentrated to give a 20 to  50° by weight concentration of dyestuff or optical brightening agent.	40
-	15. A preparation according to claim 13 which is concentrated to dryness.  16. A preparation according to any one of claims 13 to 15 whenever obtained by a process as claimed in any one of claims 1 to 5 and 11	

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